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FILE COVERS 1964 TO 22 Jan 2003 (20030122/ED)

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The Indexing Template (TD) field is available for some records starting with 940901/ED. Enter HELP TEMPLATE at an arrow prompt (=>) for information on how to use this field.

This file contains CAS Registry Numbers for easy and accurate substance identification.

=> s (catalyst (1) zsm-50 zeolite (1) phosphorus (1) (nickel or cobalt) (1) (molybdenum or tungsten))/lt

100961 CATALYST/LT

63 ZSM-50 ZEOLITE/LT

17390 PHOSPHORUS/LT

22475 NICKEL/LT

18138 COBALT/LT

16374 MOLYBDENUM/LT

9212 TUNGSTEN/LT

L2 0 (CATALYST (L) ZSM-50 ZEOLITE (L) PHOSPHORUS (L) (NICKEL OR COBAL T) (L) (MOLYBDENUM OR TUNGSTEN))/LT

=> s (catalyst (1) zsm-50 zeolite (1) phosphorus)/lt

100961 CATALYST/LT

63 ZSM-50 ZEOLITE/LT

17390 PHOSPHORUS/LT

7 (CATALYST (L) ZSM-50 ZEOLITE (L) PHOSPHORUS)/LT

=> d 1-7

L3

L3 ANSWER 1 OF 7 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION INC.

AN 2001:6400 ENCOMPPAT; ENCOMPPAT2

DN P200108921

TI Process for the production of gasolines of improved octane index by successive operations of hydroisomerisation, separation of isoparaffins and isomerization

IN BENAZZI E; BIGEARD P; CSERI T; MARCHAL-GEORGES N; BIGEARD P H

PA INST FRANCAIS DU PETROLE

PI EP 1088879 20010404

DS AL; AT; BE; CH; CY; DE; DK; ES; FI; FR; GB; GR; IE; IT; LI; LT; LU; LV; MC; MK; NL; PT; RO; SE; SI

AI EP 2000-402632 20000922

PRAI FR 1999-12337 19990930

OS DERWENT 2001228378

LA French

ANSWER 2 OF 7 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION INC.

AN 2001:3687 ENCOMPPAT; ENCOMPPAT2

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P200105248
 DN.
 TI
     Production of base oil from hydrocarbon charging material,
     performing simultaneous hydrogenation and isomerization of charging
     material and contact deparaffination of the effluent under specific
     conditions
PA
     INST FRANCAIS DU PETROLE
PΙ
     JP 2000345170 20001212
ΑI
     JP 2000-132785 20000501
PRAI FR 2000-2364 20000224
     FR 1999-5494 19990429
OS
     DERWENT 2001129394
L3
     ANSWER 3 OF 7 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION
     INC.
ΑN
     2001:2301 ENCOMPPAT; ENCOMPPAT2
DN
     P200103332
TI
     Production of oils and middle distillates, useful as lubricants, involves
     successive conversion of hydrocarbons by hydroisomerization and catalytic
     deparaffination
IN
     BENAZZI E; CSERI T; GUERET C; MARCHAL G N; MARION P
PΑ
     INST FRANCAIS DU PETROLE
PI
     FR 2792945 20001103
     FR 1999-5494 19990429
ΑI
PRAI FR 1999-5494 19990429
OS
     DERWENT 2001073431
L3
     ANSWER 4 OF 7 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION
AN
     2001:600 ENCOMPPAT; ENCOMPPAT2
DN
     P200100894
TΤ
     Base oil and middle distillate production comprises successive conversions
     of hydro-isomerization and catalytic deparaffination
     BENAZZI E; CSERI T; GUERET C; KASZTELAN S; MARCHAL G N; MARION P
ΙN
PA
     INST FRANCAIS DU PETROLE
PΙ
     FR 2792946 20001103
ΑI
     FR 1999-5496 19990429
PRAI FR 1999-5496 19990429
OS
     DERWENT 2001001274
     ANSWER 5 OF 7 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION
L3
     1999:13485 ENCOMPPAT; ENCOMPPAT2
AN
DN
     9913005
     Improving catalytic activity of small and medium pore acidic zeolite
TI
     catalysts useful in hydrocarbon cracking
IN
     CAO G; CHEN T; MARTENS L R M; SHAH M J; WHITE J L
PA
     EXXON CHEM PATENTS INC
PΙ
     WO 9946043 19990916
     AL; AM; AT; AU; AZ; BA; BB; BG; BR; BY; CA; CH; CN; CU; CZ; DE; DK; EE;
DS
     ES; FI; GB; GD; GE; GH; GM; HR; HU; ID; IL; IN; IS; JP; KE; KG; KP; KR;
     KZ; LC; LK; LR; LS; LT; LU; LV; MD; MG; MK; MN; MW; MX; NO; NZ; PL; PT;
     RO; RU; SD; SE; SG; SI; SK; SL; TJ; TM; TR; TT; UA; UG; UZ; VN; YU; ZW;
     AT; BE; CH; CY; DE; DK; EA; ES; FI; FR; GB; GH; GM; GR; IE; IT; KE; LS;
     LU; MC; MW; NL; OA; PT; SD; SE; SL; SZ; UG; ZW
     WO
        1999-US5059 19990309
PRAI US
        1998-38649 19980311
OS
     DERWENT 99571703
LΑ
     English
L3
     ANSWER 6 OF 7 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION
AN
     93:4511 ENCOMPPAT; ENCOMPPAT2
DN
     9315343
ΤI
     Reclaiming-thermoset polymer e.g. polyester resin, for chemical
     intermediates - by heating in presence of zeolite-contg. particulate
     catalyst, yielding volatile lower molecular wt. organic cpds. for solvent
     or fuel and reusable filler
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COZZONE G E; GAFFNEY A M; NES C A; LEYSHON D W; SOFRANKO
IN.
PA
     ARCO CHEM TECHNOLOGY LP
PΙ
     US 5192809 930309
AI US 1992-860638 920330
PRAI US 1992-860638 920330
     DERWENT 93100362
     ANSWER 7 OF 7 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION
     INC.
AN
     89:4335 ENCOMPPAT; ENCOMPPAT2
     8911322
DN
TI
     Enhancing ion exchange capacity of a titanic silicate - without enhancing
     its acid activity, by treatment with aq. alkaline soln
PA
     Mobil Oil Corp
        4828812 890509
PΙ
     US
PRAI US 1987-138972 871229
     DERWENT 89165139
os
=> s (catalyst (1) zeolite (1) phosphorus (1) (nickel or cobalt) (1) (molybdenum or
tungsten))/lt
        100961 CATALYST/LT
         16232 ZEOLITE/LT
         17390 PHOSPHORUS/LT
         22475 NICKEL/LT
         18138 COBALT/LT
         16374 MOLYBDENUM/LT
          9212 TUNGSTEN/LT
           135 (CATALYST (L) ZEOLITE (L) PHOSPHORUS (L) (NICKEL OR COBALT) (L)
L4
               (MOLYBDENUM OR TUNGSTEN))/LT
\Rightarrow s l1 and l4
           10 L1 AND L4
=> d 1-10
     ANSWER 1 OF 10 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION
     INC.
AN
     1999:11672 ENCOMPPAT; ENCOMPPAT2
DN
     9912777
TI
     Dewaxing of hydrocarbon feedstocks
     HOWELL R L; ROSENBAUM J M
IN
PA
     CHEVRON USA INC
     WO 9929810 19990617
PI
DS
     AL; AM; AT; AU; AZ; BA; BB; BG; BR; BY; CA; CH; CN; CU; CZ; DE; DK; EE;
     ES; FI; GB; GE; GH; GM; HR; HU; ID; IL; IS; JP; KE; KG; KP; KR; KZ; LC;
     LK; LR; LS; LT; LU; LV; MD; MG; MK; MN; MW; MX; NO; NZ; PL; PT; RO; RU;
     SD; SE; SG; SI; SK; SL; TJ; TM; TR; TT; UA; UG; UZ; VN; YU; ZW; AT; BE;
     CH; CY; DE; DK; EA; ES; FI; FR; GB; GH; GM; GR; IE; IT; KE; LS; LU; MC;
     MW; NL; OA; PT; SD; SE; SZ; UG; ZW
     WO 1998-US26112 19981209
AΤ
PRAI US 1997-988287 19971210
os
     DERWENT 99518207
LΑ
     English
L5
     ANSWER 2 OF 10 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION
     INC.
     92:3141 ENCOMPPAT; ENCOMPPAT2
AN
DN
     New SM-3 silico-alumino-phosphate zeolite(s) - useful in hydrocracking and
ΤI
     dewaxing catalysts
     Chevron Research Co
PA
     US 5087347 920211
PΙ
PRAI US 1990-550937 900711
OS
     DERWENT 92072113
L5
     ANSWER 3 OF 10 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION
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INC. 91:7000 ENCOMPPAT; ENCOMP ANDN 9112273 TI. Catalyst compsn. - comprises gallio-silicate molecular sieve having zeolite L structure, useful for conversion of hydrocarbon(s) Union Oil Co California PA PΙ US 5035868 910730 PRAI US 1989-458351 891228 **DERWENT 91245420** os ANSWER 4 OF 10 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION INC. 91:1370 ENCOMPPAT; ENCOMPPAT2 AN 9110490 DN ΤI De-waxing of gas oils and kerosene(s) - by use of a crystalline synthetic zeolite of a ferri silicate type Institut Français Du Petrole Des Car PA EP 404666 901227 PI AT; BE; DE; ES; FR; GB; IT; NL DS PRAI FR 1989-8358 890621 **DERWENT 91001669** OS 1.5 ANSWER 5 OF 10 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION TNC. AN91:64 ENCOMPPAT; ENCOMPPAT2 DN 9110037 TΙ Catalytic dewaxing of a hydrocarbon feedstock - using a catalyst containing a selected silico alumino-phosphate molecular sieve and a hydrogenation component PA UOP Inc US 4960504 901002 PΙ PRAI US 1988-158667 880222 DERWENT 90319746 OS L5 ANSWER 6 OF 10 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION INC. AN 89:3168 ENCOMPPAT; ENCOMPPAT2 DN 8911052 TΙ Catalyst contg. nickel oxide and cracking component - esp. Y zeolite, is useful in gas oil hydrocracking, giving gasoline fractions of increased octane number PA Union Oil Co California US 4816538 890328 PΙ PRAI US 1987-81472 870804 OS DERWENT 89113939 L5 ANSWER 7 OF 10 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION INC. 86:2162 ENCOMPPAT; ENCOMPPAT2 ΑN DN 8611823W TТ DEWAXING PROCESS USING CATALYST CONTG. NON ZEOLITIC MOLECULAR SIEVE - AND OPT. HYDROGENATION COMPONENT, ACTIVE ALUMINOSILICATE ZEOLITE, AND INORGANIC OXIDE MATRIX PΑ UNION CARBIDE CORP WO 8603770 PIDS AU; JP PRAI US 1984-682942 841218 OS DERWENT 86182904 L5 ANSWER 8 OF 10 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION INC.

DEWAXING PROCESS USING CATALYST CONTG. NON ZEOLITIC MOLECULAR SIEVE - AND

OPT. HYDROGENATION COMPONENT, ACTIVE ALUMINOSILICATE ZEOLITE, AND

AN

DN

ΤI

PA

8611823U

86:2161 ENCOMPPAT; ENCOMPPAT2

INORGANIC OXIDE MATRIX

UNION CARBIDE CORP

PI. WO 8603770 DS. AU; JP

PRAI US 1984-682942 841218

OS DERWENT 86182904

- L5 ANSWER 9 OF 10 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION INC.
- AN 86:2159 ENCOMPPAT; ENCOMPPAT2

DN 8611822

- TI HYDROCRACKING, USING CATALYST CONTG. SILICO ALUMINO-PHOSPHATE MOLECULAR SIEVE, HYDROGENATION COMPONENT, AND OPT. ZEOLITE, GIVES INCREASED ISON RATIO AND RESEARCH OCTANE NUMBER IN GASOLINE PROD
- PA UNION CARBIDE CORP
- PI WO 8603694
- DS AT; BE; CH; DE; FR; GB; IT; LU; NL; SE; AU; FI; JP
- PRAI US 1984-682946 841218
- OS DERWENT 86182850
- L5 ANSWER 10 OF 10 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION INC.
- AN 86:2071 ENCOMPPAT; ENCOMPPAT2
- DN 8611719
- TI CATALYTIC DEWAXING OF HYDROCARBON FEEDS USING SILICO-ALUMINO-PHOSPHATE ZEOLITE CATALYST
- PA UNION CARBIDE CORP
- PI EP 185329
- DS AT; BE; CH; DE; FR; GB; IT; LI; LU; NL; SE
- PRAI US 1984-683246 841218
- OS DERWENT 86163348

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- L5 ANSWER 1 OF 10 ENCOMPPAT COPYRIGHT 2003 ELSEVIER ENGINEERING INFORMATION INC.
- NOVELTY Two stage process with fractionation, in which the bottoms AR fraction is recycled to the feedstock, increased yield and pour point reduction in dewaxing of lube oils. DETAILED DESCRIPTION - Conversion of hydrocarbon oil involves: (a) contacting a hydrocarbon oil feedstock in the presence of added hydrogen gas with catalyst system comprising intermediate pore size silicoaluminophosphate mol. sieve and hydrogenation component, with at least part of the feedstock being converted, (b) passing at least part of the converted feedstock to a fractionation to produce at least one overhead fraction and one bottoms fraction and (c) mixing at least part of the bottoms fraction with the hydrocarbon oil feedstock. An INDEPENDENT CLAIM is included for the dewaxing of the hydrocarbon oil using the above process. USE - For use in dewaxing of lube oil feedstocks. ADVANTAGE - Increases yield and/or reduces pour point and/or viscosity of dewaxed lube oils or middle distillates. Dwg (40pp Dwg.No.1/1)